

# Problem 1.

# TA Session

**20-5.** In this problem, we will prove that Equation 20.5 is valid for an arbitrary system. To do this, consider an isolated system made up of two equilibrium subsystems, A and B, which are in thermal contact with each other; in other words, they can exchange energy as heat between themselves. Let subsystem A be an ideal gas and let subsystem B be arbitrary. Suppose now that an infinitesimal reversible process occurs in A accompanied by an exchange of energy as heat  $\delta q_{\text{rev}}$  (ideal). Simultaneously, another infinitesimal reversible process takes place in B accompanied by an exchange of energy as heat  $\delta q_{\text{rev}}$  (arbitrary). Because the composite system is isolated, the First Law requires that

$$\delta q_{\text{rev}}(\text{ideal}) = -\delta q_{\text{rev}}(\text{arbitrary})$$

Now use Equation 20.4 to prove that

$$\oint \frac{\delta q_{\text{rev}}(\text{arbitrary})}{T} = 0$$

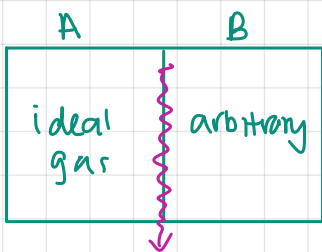
Therefore, we can say that the definition given by Equation 20.4 holds for any system.

Equation 20.5  $\rightarrow \int \frac{\delta q_{\text{rev}}}{T} = 0$  infinitesimal reversible process } both A & B  
 pg 821 exchange of  $\delta q_{\text{rev}}$

$$\delta q_{\text{rev}}(\text{ideal}) = -\delta q_{\text{rev}}(\text{arbitrary})$$

$$\delta q_{\text{rev}}(A) = -\delta q_{\text{rev}}(B)$$

show  $\oint \frac{\delta q_{\text{rev}}(\text{arbitrary})}{T} = 0$



heat transfer

From first law we derive

use eq 20.1  $\rightarrow \delta q_{\text{rev}} = dU - \delta w_{\text{rev}} = C_v(T) dT + PdV$   
 $= C_v(T) dT + \frac{nRT}{V} dV$

$$\therefore \delta q_{\text{rev}}(B) = - \underbrace{C_v(T) dT + \frac{nRT}{V} dV}_{q_{\text{rev}}(A)}$$

$$\frac{\delta q_{\text{rev}}(B)}{T} = - \frac{C_v}{T} dT + \frac{nRT}{T^2} dV$$

$$= d \left[ \int -\frac{C_v(T)}{T} dT - nR \int \frac{dV}{V} + c \right]$$

\* Cyclic integral of state function = 0

$$\oint dY = 0$$

$$\oint dY = \int_1^2 dY + \int_2^1 dY = Y_2 - Y_1 + (Y_1 - Y_2) = 0$$

therefore:  $\oint \frac{\delta q_{rev} \text{ (arbitrary)}}{T} = 0$

## Problem #2

Calculate  $\Delta H$  :  $\Delta S$  for system & surrounding when 1 mol of water is vaporized at  $100^\circ\text{C}$ . Value of  $\Delta H_{vap} = 40.65 \text{ kJ/mol}$   
Comment on sign of  $\Delta S_{vap}$

$$\Delta H_{sys} = \Delta H_{vap}$$

$$\Delta H_{sys} = -\Delta H_{surr}$$

$$\Delta S = \frac{\delta q_{rev}}{T} \text{ where } \Delta H = q$$

$$\text{so, } \Delta S = \frac{\Delta H_{sys}}{T}$$

$$\text{and } \Delta S_{sys} = -\Delta S_{surr}$$

at const. pressure,  $\Delta H = \Delta U + \Delta(PV)$   
 $\Delta U = q + w = q - P\Delta V$

so,  $\Delta H = q - \cancel{P\Delta V} + \overset{\text{bc constant}}{P\Delta V}$

so,  $\Delta H = q$  at constant pressure

\* convert to Kelvin

### Problem #3

Calculate  $\Delta S$  of system and surr when 1 mol of ideal monoatomic gas doubles in volume.

a) isothermal reversible expansion Page 822

$$\begin{array}{l} \downarrow \\ \Delta T = 0 \\ \Delta U = 0 \end{array} \quad \left[ \Delta S = \int \frac{q_{rev}}{T} \Rightarrow \int_{v_1}^{v_2} \frac{1}{T} \frac{nRT_1}{V} dV \Rightarrow nR \int_{v_1}^{v_2} \frac{dV}{V} \right]$$

I got this from book

$$\Delta S = nR \ln\left(\frac{2V}{V}\right)$$

$$\Delta S_{system} = -\Delta S_{surr}$$

b) isothermal, irreversible, in vacuum

$$\begin{array}{l} \downarrow \\ \Delta T = 0 \\ \Delta U = 0 \end{array}$$

$$\begin{array}{l} \downarrow \\ P_{ex} = 0 \\ W = 0 \end{array}$$

$$\Delta S_{surr} = \frac{q_{surr}}{T} = -\frac{q_{sys}^{actual}}{T}$$

$$irrev \Delta S_{system} = \overset{rev}{\Delta S_{system}} = nR \ln\left(\frac{2V}{V}\right)$$

$$\Delta S_{surr} = \frac{q_{surr}}{T} \quad \text{where} \quad \begin{array}{l} \Delta U = q_{surr} + W \\ 0 = q_{surr} + 0 \quad \text{so,} \\ q_{surr} = 0 \end{array} \quad \Delta S_{surr} = 0$$

In vacuum means  $\Delta S_{surr} = 0$

### c) adiabatic reversible expansion

$$\Delta q = 0$$

$$\Delta S = \frac{q_{rev}}{T}$$

$$\Delta S_{system} = -\Delta S_{surr}$$

### d) adiabatic irreversible expansion into a vacuum

$\Delta q = 0$  \* from notes, since  $\Delta S$  is a state function, we change the system to make it reversible, so we can use  $\Delta S = \frac{q_{rev}}{T}$  because  $\Delta U = 0$ , we use isothermal reversible

$$P_{ext} = 0$$

$$W = 0$$

$$\Delta S = nR \ln\left(\frac{V_2}{V_1}\right) \text{ where } \left(\frac{2V}{V}\right)$$

### Problem 4

1 mol ideal gas  
 $T_{sys} = 300K$  isothermal until  $P = P_{ext}$  (irreversible)  
 $V_i = 25L$   $V_f = 10L$   
 $T_{surr} = 300K$  find  $S_{sys}$ ,  $S_{surr}$ ,  $S_{univ}$

isothermal, irreversible

$$\Delta T = 0$$

$\Delta S$  is state function so we can use  $\Delta S_{sys} = nR \ln\left(\frac{V_2}{V_1}\right)$

$$P_{ext} = P_f \text{ where } \delta q_{sys} = \delta W = -P_f \Delta V$$

\* in this case  $\Delta S \neq 0$  and  $\Delta S_{surr} \neq \Delta S_{sys}$

$$P_f = \frac{nRT_f}{V_f} \text{ then, } W = -P_f \left(\frac{V_f}{V_i}\right)$$

$$\text{and } q = -W \text{ and } \Delta S = -\frac{\delta q_{surr}}{T}$$

$$\text{and } S_{univ} = S_{sys} + S_{surr}$$

find  $P_f$  to find  $W$  to find  $q$  to find  $S_{surr}$  where  $P_f = P_{ext}$  using ideal gas law

### Problem 5

2.5 mol ideal monoatomic gas  
 $T_i = 310K$   $P_i = 1 \text{ bar}$   
 calculate  $q$ ,  $w$ ,  $\Delta U$ ,  $\Delta H$ ,  $\Delta S$

can use  $\Delta S_{sys} = -\Delta S_{surr}$  as long as  $q \neq 0$   
 $S_{surr} = 0$  when adiabatic for prob 5,

a) gas heated to 675K and constant  $P_{\text{ext}} = 1 \text{ bar}$

First, find  $V_1$ , use  $PV = nRT \Rightarrow V_1 = \frac{nRT_1}{P_1}$  \* constant pressure

then, using **Charles's law**: at  $\Delta P = 0$ ,  $\frac{V_1}{T_1} = \frac{V_2}{T_2}$

so  $V_2 = V_1 \cdot \frac{T_2}{T_1}$  then  $w = -P_{\text{ext}} \Delta V$

$$\Delta U = \frac{3}{2} nRT$$

at constant pressure  $q = \Delta H = \Delta U + P \Delta V$   
( $\Delta U - w$ )

and since  $q = C_V nR \Delta T$ ,  $\Delta S = \int \frac{dq_{\text{rev}}}{T} = \int \frac{C_V(T)}{T} dT + \int \frac{nR}{V} dV$

$$= \frac{3}{2} nR \ln \frac{T_f}{T_i} + \frac{3}{2} nR \ln \left( \frac{V_f}{V_i} \right)$$

b)  $T_2 = 675 \text{ K}$  at constant volume,  $V_1 = V_f$

$$\Delta U = q + w \overset{w=0}{\rightarrow} \quad \frac{PV}{V} = \frac{nRT}{V}$$

$$q = \Delta U = \frac{3}{2} nR \Delta T$$

$$\Delta H = \Delta U + \Delta(PV) = \Delta U + \Delta \left( \frac{nRT}{V} \cdot V \right) = \Delta U + nR \Delta T$$

$$\Delta S = \frac{3}{2} nR \ln \frac{T_f}{T_i} + \frac{3}{2} nR \ln \left( \frac{V_f}{V_i} \right) \rightarrow 0$$

c) reversible isothermal expansion,  $P_f = 3P_i$

$$P_1 V_1 = P_2 V_2$$

$$T = 310 \text{ K}$$

$$1 \cdot V_1 = 3 \cdot V_2$$

why?  $\rightarrow$

$$\Delta T = 0$$

$$\Delta U = \frac{3}{2} nR \Delta T = 0$$

$$\Delta U = \Delta H = 0$$

$$w = -q = -nR \ln \left( \frac{V_f}{V_i} \right)$$

$$\left. \begin{array}{l} V_f = 3 \\ V_i = 1 \end{array} \right\}$$

Dropping pressure means volume goes up proportionally

$$\Delta S = \frac{3}{2} nR \ln \frac{T_f}{T_i} + nR \ln \frac{V_f}{V_i}$$